Oxidative Dimerization of Methane over BaCO₃, SrCO₃ and these Catalysts promoted with Alkali

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The yield and selectivity for formation of C₂ hydrocarbons from CH₄ and O₂ were 18.2 and 48.4% respectively over 2 g of BaCO₃ at 1073 K at a CH₄: O₂ ratio of 2.0: 1, whereas the yield and selectivity were 2.5 and 99.5% over SrCO₃ at 973 K at a CH₄: O₂ ratio of 37.9: 1.

Various ma[•]erials (PbO–Al₂O₃,¹ Li⁺–MgO,² Na⁺–MgO,³ Sm₂O₃,⁴ LaAlO₃,⁵ La₂O₃,⁶ and Li⁺–Sm₂O₃⁷) have been reported to be effective catalysts for the title reaction. Among these, alkali doped MgO has been reported to show the highest yield for C₂ compound formation.^{2,3} We studied the title reaction over a simple alkaline earth oxide and carbonate and these catalysts promoted with alkali, although alumina supported alkali earth oxides have been reported to have low activities.⁸

Reactions were performed in a conventional flow reactor (8 mm o.d.) at temperatures between 673 to 1073 K, and CH₄, air, and He flow rates of 1.5 ml min⁻¹ (4.02 mmol h⁻¹), 3.75 ml min⁻¹, and 50 ml min⁻¹ respectively. The CH₄: O₂ ratio was 2 : 1 (2CH₄ + O₂ = C₂H₄ + 2H₂O). Commercial BaO and CaO were crushed and sieved to a suitable size (20 mesh). Hydrated and dried SiO₂ (Cab-O-Sil) was also crushed and sieved (20 mesh). ZnO (Kadox), anatase TiO₂ (MCB), MgO (Soekawa), BaCO₃, and SrCO₃ were mixed with water to make a slurry, partly dried, and the paste was extruded using a plastic syringe. SrO was made by baking Sr(OH)₂·8H₂O at 673 K for 4 h. Alkali metal nitrates were added to BaCO₃ or SrCO₃ in water, and the samples were dried and weighed. The reagents which are not cited were obtained through Kanto

Chemical Co. The sample (2 g) was evacuated or heated in a He flow at 773 K for 1 h and at 1073 K for 2 h and used for the reaction. The alkali metal nitrates (promoters) are considered to be decomposed to the oxides or the hydroxides during the pretreatment.

In Table 1 we summarize our results of the reaction for the various oxides, carbonates, and the promoted catalysts at the $CH_4:O_2$ ratio of 2.0:1. The yield and the selectivity are defined as $(2 \times \text{moles } C_2 \text{ hydrocarbons produced})/(\text{moles } CH_4)$ in the feed) and (2 \times moles C₂ hydrocarbons produced)/ (moles CH₄ reacted), respectively. Oxides of alkali earth elements are more effective than the other oxides studied here. The effectiveness of these catalysts increases with increasing atomic number (BaO \approx SrO > CaO > MgO). The highest yields of C2 products over SrO and BaO without alkali promoters were 16.3 and 16.6% respectively at 1073 K. However, BaO and SrO gave no CO₂ as a product during several hours of the reaction because these oxides are partly converted into their carbonates under the reaction conditions. (The decomposition temperatures of carbonates are 1613 and 1633 K for SrCO₃ and BaCO₃ respectively.) Another problem with BaO and SrO is the corrosion of the glass reactor.

In order to overcome these problems, we studied oxidative

Table 1. Activity and selectivity of the oxidative dimerization of CH₄ at 1023 and 1073 K.^a

| Catalyst (2 g) | $\begin{array}{c} 1023 \text{ K} \\ \text{Yield for } C_2 \\ \text{compounds (\%)} \end{array}$ | Selectivity for C ₂ compounds (%) | $\begin{array}{c} 1073 \text{ K} \\ \text{Yield for } \text{C}_2 \\ \text{compounds} (\%) \end{array}$ | $\begin{array}{c} \text{Selectivity} \\ \text{for } C_2 \\ \text{compounds} (\%) \end{array}$ |
|---|---|--|--|---|
| MgO | 4.4 | 11.7 | — | |
| CaO | 9.4 | 28.9 | 12.8 | 39.1 |
| SrO | 10.0 | 39.0 | 16.3 | 52.7 |
| SrCO ₃ | 8.5 | 22.7 | | |
| | (4.4) ^b | (98.0) ^b | (6.4) ^b | (92.7)ь |
| | (2.5) ^{b,c} | (99.5) ^{b,c} | | |
| SrCO ₃ -2 mol% K ^{+ d} | 5.0 | 46.5 | 11.5 | 55.5 |
| SrCO ₃ -10 mol% K+ | 4.1 | 43.9 | 8.7 | 58.2 |
| SrCO ₃ -10 mol% Rb+ | 4.0 | 30.5 | 10.1 | 37.1 |
| BaO | 15.2 | 45.4 | 16.6 | 44.6 |
| BaCO ₃ | 15.3 | 46.3 | 18.2 | 48.4 |
| | (5.1) ^b | (82.5) ^b | (7.1) ^b | (90.5) ^b |
| BaCO ₃ -2 mol% Li+ | 15.3 | 44.3 | 18.5 | 49.6 |
| BaCO ₃ -2 mol% Na+ | 16.3 | 43.5 | 15.5 | 42.5 |
| BaCO ₃ -2 mol% K ⁺ | 17.0 | 37.6 | 20.2 | 42.0 |
| BaCO ₃ -2 mol% Rb+ | 17.6 | 41.8 | 17.1 | 37.9 |
| ZnO | 0.1 | 1.0 | | |
| TiO ₂ | 0.0 | 0.0 | | |
| ZrO_2 | 0.2 | 1.0 | | |
| SiO ₂ | 0.4 | 2.0 | | |
| SiO ₂ -200 mol% Sr ²⁺ | 2.2 | 13.3 | 7.6 | 25.4 |

^a CH₄: $O_2 = 2.0:1$; selectivity = $(2 \times \text{moles } C_2 \text{ hydrocarbons produced})/(\text{moles CH}_4 \text{ reacted})$. ^b CH₄: $O_2 = 37.9:1$; selectivity = (moles carbon in C₂ hydrocarbons)/(moles carbon in all the products). ^c Reaction at 973 K. ^d Percentage molar ratio of a promoter against an unpromoted oxide or a carbonate.

dimerization over BaCO₃ and SrCO₃. The activities and the kinetic behaviour of these carbonates are almost identical to those of their oxides. The carbonates of Sr and Ba prove to be the most effective catalysts. The yield of C₂ hydrocarbon is 18.2% over BaCO₃ at 1073 K, which compares well with the best values reported previously: (19.4, 21, and 22.4% over 7 wt% Li⁺-MgO,² 10 mol% Li⁺-Sm₂O₃,⁷ and 15 mol% Na⁺-MgO³ catalysts). These carbonates are also considered to have radical centres which abstract hydrogen from CH₄ at the elevated temperature.² Since BaCO₃ and SrCO₃ are thermally stable and not corrosive, they should be the favoured catalysts for industrial use. Although the alkali promoted MgO has been reported to be the most effective catalyst,^{2,3} the alkali elements in the MgO might be lost during a long run at high temperature.

The promoter effect of alkali in the BaCO₃ and SrCO₃ catalysts was also studied as is shown in Table 1. In the case of BaCO₃, the activity of C₂ formation was improved. The highest C₂ yield (20.2%) was observed over 2 g of 2 mol% K⁺-BaCO₃ at 1073 K with a C₂ selectivity of 42%. In the case of SrCO₃, the activity is depressed a little, whereas the selectivity is improved. The maximum C₂ selectivity observed was 58.2% for 2 g of 10 mol% K⁺-SrCO₃ at 1073 K at a CH₄: O₂ ratio of 2.0:1.

When the CH₄: O_2 ratio was increased from 2.0:1 to 37.9:1 (flow rate of CH₄, air, He = 12.9, 1.70, 50 ml min⁻¹), the selectivity for C₂ compounds increased for the carbonate catalysts, as is shown in Table 1. In particular, SrCO₃ improved in selectivity from 25.6 to 98.0% at 1023 K and even

to 99.5% at 973 K, a value higher than any previously reported.¹⁻⁷

In summary, for stable compounds which contain no additives $BaCO_3$ and $SrCO_3$ were found to be among the most effective catalysts for the oxidative dimerization of methane. These carbonates can be improved in their activity and selectivity when they are doped with alkali.

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